# OPERATING SUMMARY

# STRATFORD

water pollution control plant

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ONTARIO WATER
RESOURCES COMMISSION

ONTARIO WATER RESOURCES COMMISSION

Division of Plant Operations



Water management in Ontario

Ontario Water Resources Commission 135 St. Clair Ave.W. Toronto 195 Ontario

The operating efficiency and financial status of the water pollution control facilities operated for you in 1969 are presented in the following pages.

The regional operations engineer's comments and the statistical data will assist you in gauging the plant's level of performance. A new flow chart and up-to-date design data are also provided.

Various divisions and sections within the Commission have cooperated in providing what we trust is an accurate and concise annual operating summary.

D.S. Caverly,

General Manager.

D. A. McTavish, P. Eng.,

Director,

Division of Plant Operations.

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# STRATFORD water pollution control plant

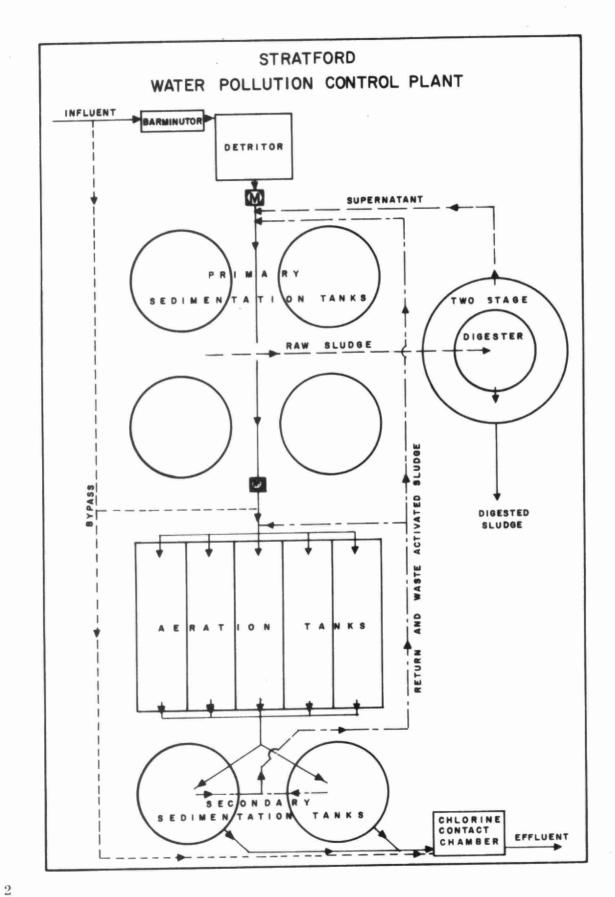
operated for

THE CITY OF STRATFORD

by the

ONTARIO WATER RESOURCES COMMISSION

1969 ANNUAL OPERATING SUMMARY



#### DESIGN DATA

PROJECT NO.	2-0002-57	TREATMENT Activated Sludge
DESIGN FLOW	6.0 mgd	DESIGN POPULATION 30,000
BOD - Raw Sewage - Removal	140 mg/l 90%	SS – Raw Sewage 250 mg/l – Removal 95%

#### PRIMARY TREATMENT

#### Comminution

Type: Barminutor

Size: One Model C (36")

#### Grit Removal

Type: Dorr detritor

Size: One 20' x 20' x 1' (2,500 gal)

Retention: 0.9 min

#### Primary Sedimentation

Type: Infilco

Size: Four 80' dia x  $10\frac{1}{2}$ ' swd (1.32)

mil gal)

NOTE: Two used for storm flows only

Retention: 2.7 hr (2 cl)

Loading: Surface, 600 gal/ft<sup>2</sup>/day

Weir, 12,000 gal/ft/day

#### SECONDARY TREATMENT

#### Aeration Tanks

Type: Diffused air; triple-pass

Size: Five  $85\frac{1}{2}$ ' x 25' 8'' (avg) x 13'

(0.97 mil gal)

Retention: 3.9 hr

#### Diffusers

Type: Activated Sludge Ltd.

Alundum Domes

#### Air Supply

Type: Roots-Connersville Size: Three 1750 cfm

#### Secondary Sedimentation

Type: Infilco

Size: Two 80' dia x 11' 3" swd

(0.705 mil gal)

Retention: 2.7 hr

Loading: Surface, 600 gal/ft<sup>2</sup>/day

Weir, 12,000 gal/ft/day

#### CHLORINATION

#### Chlorine Contact Chamber

Size: 67' x 27' x 8' (90,000 gal)

Retention: 22 min

#### Chlorinator

One F & P 500 lb/day

#### OUTFALL

- to Avon River

#### SLUDGE HANDLING

#### Digestion System - Heated, two-stage

Type: Gas mixed

Size: One 73' dia x 26' swd (100,000 cu ft

or 0.624 mil gal)

#### Primary Stage (inner)

Size: 67,600 cu ft

Loading: 2.8 lb/cu ft/mo

#### Secondary Stage (outer ring)

Size: 32,400 cu ft

Total Loading: 1.9 lb/cu ft/mo



#### GENERAL

During 1969 a total flow of 1,322.5 million gallons was treated at a cost of \$75,996.47 or \$57.46 per million gallons, compared with \$56.30 in 1968. The total flow in 1969 of 1,322.5 million gallons was an increase of 7.3% from 1968. The cost of BOD removed was six cents a pound.

The consulting engineer has submitted a proposal for expansion of the plant and it is expected that plans will be finalized in 1970.

#### PLANT FLOWS and CHLORINATION

In 1969, the plant's average daily flow of 3.6 mil. gal. was 60% of the design flow of 6.0 mgd. The flow was as low as 1.1 mgd and higher than 11 mgd during the year, but the plant's capacity was exceeded only 9% of the time. In 1968, the design flow of 4.0 mgd was exceeded 40% of the time.

Despite the increase in flows, the amount of grit removed was 40 cu. ft. per month. The average dosage rate required to produce a chlorine residual of 0.5 milligrams per litreafter 15 minutes' contact was 1.7 mg/l.

#### PLANT EFFICIENCY

The average raw sewage strengths of 113 mg/l for BOD and 172 mg/l for

suspended solids showed a substantial decrease from 1968 strengths of 282 and 232 mg/l respectively. Raw sewage BOD loading exceeded the design loading 19% of the time, while suspended solids loading exceeded design 11% of the time.

Reductions of 92% BOD and 93% suspended solids were experienced in 1969 compared with 95% for each in 1968, bringing the final effluent well within the OWRC objectives.

Average final effluent BOD and suspended solids concentrations were 9 and 12 mg/l, lower than the OWRC objectives of 15 mg/l for each. These objectives were exceeded 5% of the time for BOD and 25% of the time for suspended solids.

#### SLUDGE DIGESTION

The volatile solids reductions was 29.4%, 0.4% higher than in 1968. The total solids concentration in the raw sludge of 7.0% was slightly higher than that of the previous year. The digester sludge total solids concentration in 1969 was 6.1%, slightly higher than 1968.

A total of 13,977 cubic yards of sludge was disposed of during 1969.

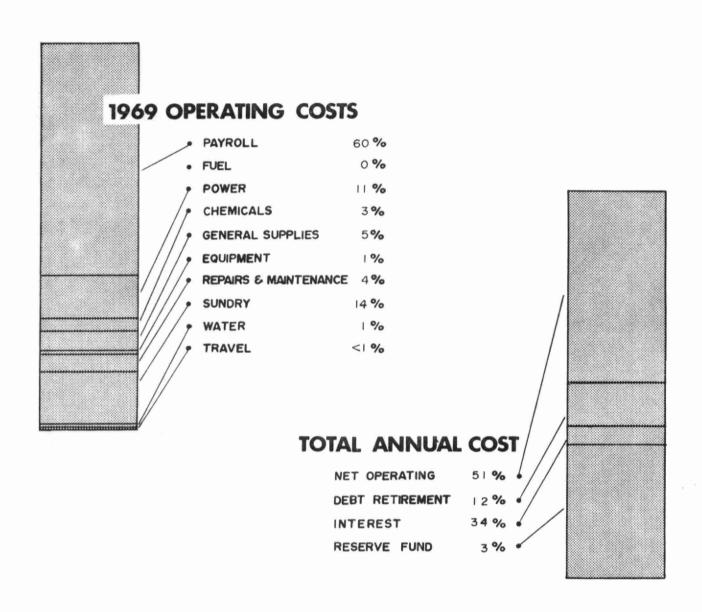
#### **CONCLUSIONS**

The plant produced an excellent effluent with BOD and suspended solids concentrations below the OWRC objectives.

Average daily flows of 3.38 million gallons were approximately the same as in 1968.

# PROJECT COSTS

NET CAPITAL COST (Final)	\$925,309.42
DEDUCT - Payments from Municipality	309.42
Long Term Debt to OWRC	\$ <u>925,000.00</u>
Debt Retirement Balance at Credit (Sinking Fund) December 31, 1969	\$ <u>279,787.87</u>
Net Operating Debt Retirement Reserve Interest Charged	\$ 75,996.47 18,667.00 3,716.53 51,785.99
TOTAL	\$ <u>150,165.99</u>
RESERVE ACCOUNT	
Balance (d) January 1, 1969	\$ 76,657.25
Deposited by Municipality	3,716.53
Interest Earned	4,423.47
	\$ 84,797.25
Less Expenditures	352.15
Balance @ December 31, 1969	\$ 84,445.10



### **Yearly Operating Costs**

YEAR	MILLION GALLONS TREATED	TOTAL OPERATING COSTS	COST PER MILLION GAL	COST PER LB OF
1965	1142.5	\$57,079.98	\$49.96	3 cents
1966	1120.8	59,148.93	52.77	2 cents
1967	1586.6	65,593.65	41.37	2 cents
1968	1232.1	69,371.20	56.30	2 cents
1969	1322.5	75,996.47	57.46	6 cents

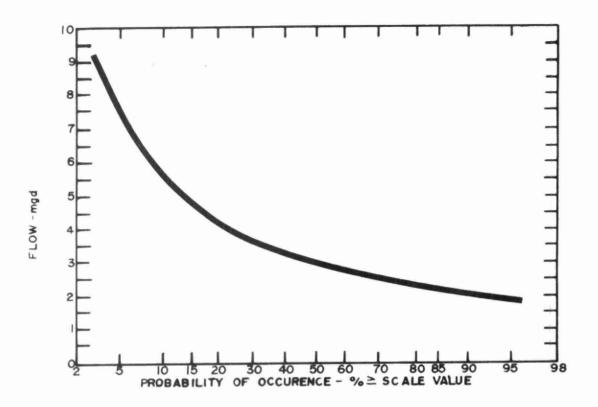
# Monthly Operating Costs

MONTH	TOTAL EXPENDITURE	PAYROLL	CASUAL PAYRO_L	FUEL	POWER	CHEMICALS	GENERAL SUPPLIES	EQUIPMENT	REPAIRS and	SUNDRY *	₩AŤER	TRAVEL.
JAN	6031.36	4915.57	-	-	741.88	-	29.03	-	259.54	23.24	53.40	8.70
FEB	7525.69	3264.47	_		808.68	2131.50	202.55	38.85	295.98	718.41	53.40	11.85
MAR	5609.57	3251.44	-	38.26	684.28	-	249.29	-	109.95	1212.30	53.40	10.65
APR	5204.45	3389.09	=	-	639.08	-	269.07	449.99	-	393.47	53.40	10.65
MAY	5842.00	3711.70	158.26	(38.26)	725.88	-	405.73	101.90	109.56	604.67	53.41	9.15
JUNE	6980.27	3936.56	364.24	_	635.08	-	441.88	-	44.47	1484.33	53.41	20.30
JULY	5596.49	3388.50	125.02	-	625.88	101.72	286.73	-	142.13	773.36	53.41	99.74
AUG	7328.80	5028.74	297.95	-	666.28	-	261.70	-	-	920.72	53.41	-
SEPT	5708.77	3383.73	239.69	_	636.28	-	489.64	-	65.38	819.49	53.41	21.15
ост	6132.67	3503.33	-	-	593.35	-	641.09	-	343.57	898.62	53.41	99.30
NOV	4508.43	3365.59	_	-	634.95	-	234.23	54.22	57.24	95.44	53.41	13.35
DEC	9527.67	3189.88	-	-	1376.30	-	322.41	-	1777.62	2745.64	106.82	9.00
TOTAL	75996.47	44328.60	1285.16	-	8767.92	2233.22	3833.35	644.96	3205.44	10689.69	694.29	313.84

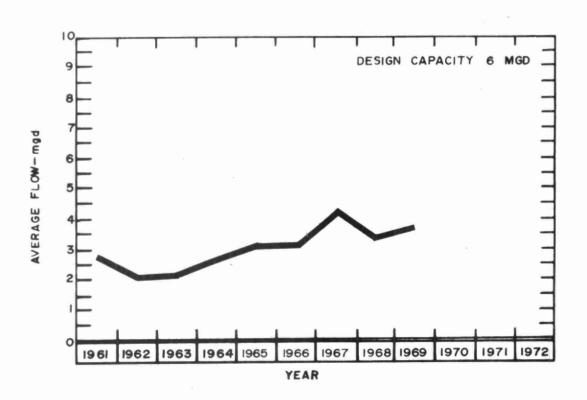
BRACKETS INDICATE CREDIT

\* SUNDRY INCLUDES SLUDGE HAULAGE COSTS WHICH WERE \$8905.47

PROCESS DATA

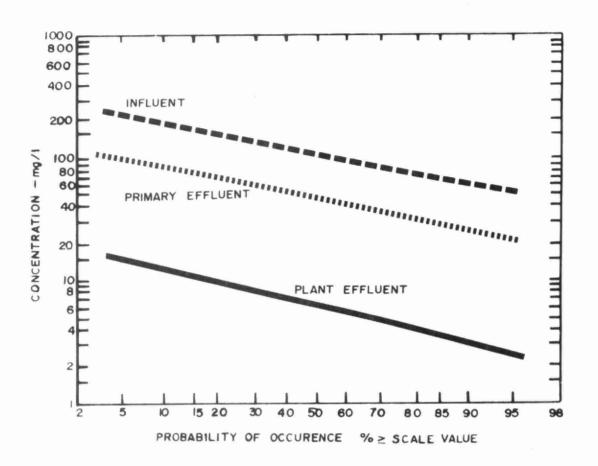


# FLOWS

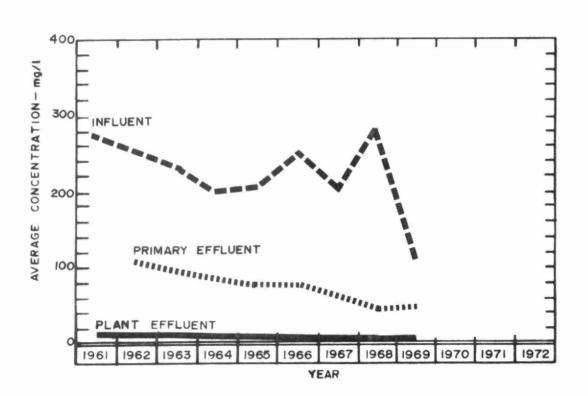


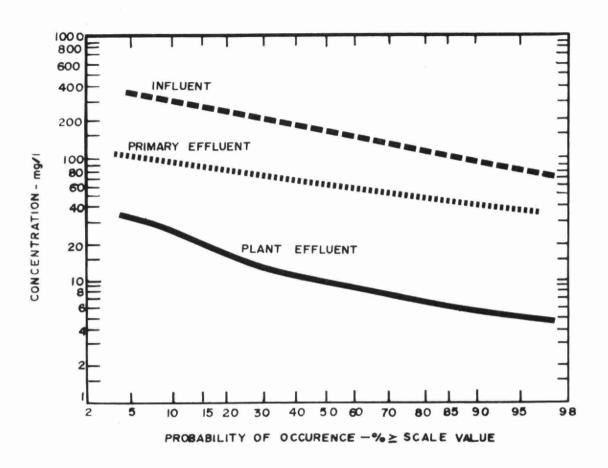
# **PLANT EFFICIENCY**

	ВІОС	HEM ICA	AL OXYG	EN DEMAND		SUSP	ENDED S	SOLIDS	GRIT
MONTH	INF.	EFF.	R	EDUCTION	INF.	EFF.	RE	DUCTION	REMOVAL
	mg/i	mg/l	%	10 <sup>3</sup> pounds	mg/I	mg/I	%	10 <sup>3</sup> pounds	cu ft
JAN	83	7	92	90.	245	17	93	270.	82
FEB	95	25	74	60.	155	8	94	127.	51
MAR	140	5	96	225.	110	5	95	175.	26
APR	205	9	96	326.	245	13	95	386.	44
MAY	90	7	92	109.	120	15	88	138.	26
JUNE	95	5	95	96.	148	7	95	150.	18
JULY	75	5	93	64.	110	5	95	96.	40
AUG	60	8	87	46.	100	5	95	85.	70
SEPT	112	9	92	78.	130	13	90	89.	34
ост	180	10	94	154.	400	33	92	332.	27
NOV	130	10	92	135.	160	10	94	168.	51
DEC	89	5	94	74.	140	10	93	114.	28
TOTAL	-	-	-	-	-	-	-	-	497
AVERAGE	113	9	92	121.	172	12	93	178.	41

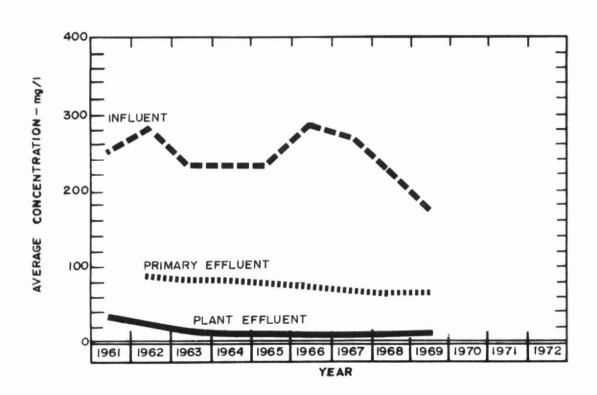


# BIOCHEMICAL OXYGEN DEMAND





# SUSPENDED SOLIDS

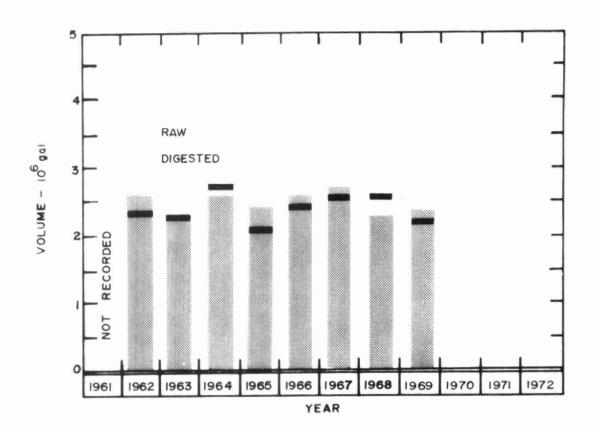


# PLANT FLOWS and CHLORINATION

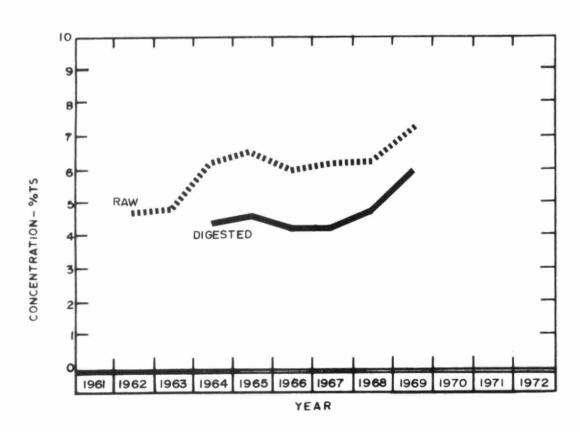
MONTH	TOTAL FLOW	AVERAGE DAILY FLOW mil gal	MAXIMUM DAILY FLOW mil gal	MINIMUM DAILY FLOW mil gal	CHLORINE USED	DOSAGE mg/l
	mii gui	mii yui	ant you	ann gui	, o position	97.
JAN	118.5	3.82	11.2	1.2	1.74	1,5
FEB	86.2	3.04	7.7	2.1	1.50	1.7
MAR	166.6	5.37	10.8	2.2	2.16	1.3
APR	166.4	5.54	10.4	3.3	2.04	1.2
MAY	131.2	4.23	9.5	2.1	1,96	1,5
JUNE	106.4	3.55	4.7	2.4	1.87	1.8
JULY	91.1	2.94	4.8	2.1	1.80	2.0
AUG	89.3	2.88	6.2	1.9	1.70	1.9
SEPT	76.2	2.54	3.6	1.1	1.64	2.2
ост	90.4	2.91	4.8	1.6	2.01	2.2
NOV	112.2	3.7	8.8	2.2	1.97	1.8
DEC	88.0	2.8	4.3	1.9	1.82	2.1
TOTAL	1322.5	-	-	-	22.21	-
AVERAGE	-	3.6	-	-	1.85	1.7

# **AERATION**

		AERATI	ON INF.	SECOND	Y. EFF.				
MONTH	AVG DAILY FLOW mil gal	B O D	SS CONCN mg/l	B O D	SS CONCN mg/l	M L S S CONCN mg/l	F/M ib BOD ib MLSS	AIR USED	WASTE SLUDGE 10 <sup>3</sup> pounds
JAN	3.21	65	65	7	17	2470	.09	1987	37.
FEB	3.03	58	65	25	8	2650	.07	1792	44.
MAR	4.85	60	80	5	5	2680	.12	1237	52.
APR	5.10	59	55	9	1	2360	.14	1215	43.
MAY	4.08	27	50	7	15	2560	.05	3546	61.
JUNE	3.53	34	43	5	7	2550	.05	2932	39.
JULY	2.93	45	70	5	5	2590	.05	2623	35.
AUG	2.81	42	65	8	5	2320	.05	3591	92.
SEPT	2.54	57	85	9	13	1870	.09	2789	.43
ост	2.91	55	80	10	33	1660	.10	2826	27.
NOV	3.00	47	45	10	10	2250	.07	3372	36.
DEC	2.60	38	45	5	10	2120	.05	4340	40.
TOTAL	-	-	-	-	-	-	-	-	-
AVERAGE	3.38	49	62	9	9	2340	.08	2688	46.



# DIGESTION



# **SLUDGE DIGESTION and DISPOSAL**

	RAW	SLUDG	Ε	DIGEST	ED SL	JDGE	SUPERN	ATANT	SLUDGE	DISPOSAL
MONTH	VOLUME	TOTAL SOLIDS	1 1	VOLUME	TOTAL SOLIDS		VOLUME	TOTAL SOLIDS	DEWATERED	LIQUID
	10 <sup>3</sup> gal	%	%	10 <sup>3</sup> gal	%	%	IO gal	%	cu yd	cu yd
JAN	209.	6.8	71	178.	4.2	63	-	-	0	1057
FEB	243.	7.6	72	267.	5.0	58	-	-	0	1568
MAR	179.	7.7	69	94.	4.8	60	-	-	0	546
APR	205.	7.4	61	120.	4.6	51	-	-	0	714
MAY	172.	7.1	70	233.	4.3	54	-	-	0	2009
JUNE	169.	7.0	74	166.	-	-	-	-	0	1043
JULY	171.	7.0	56	204.	18.0	63	-	-	0	1253
AUG	215.	7.6	61	186.	6.1	63	-	-	0	1106
SEPT	212.	5.9	71	208.	6.5	60	-	-	0	1218
ост	221.	6.4	75	184.	3.9	62	-	-	0	1083
NOV	204.	6.9	72	165.	4.4	63	-	-	0	980
DEC	218.	6.1	74	236.	4.9	67	-	-	0	1400
TOTAL	2418.	-	-	2241.	-	-	-	-	0	13977
AVERAGE	202.	7.0	68	187.	6.1	60	-	-	0	1165

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Water management in Ontario